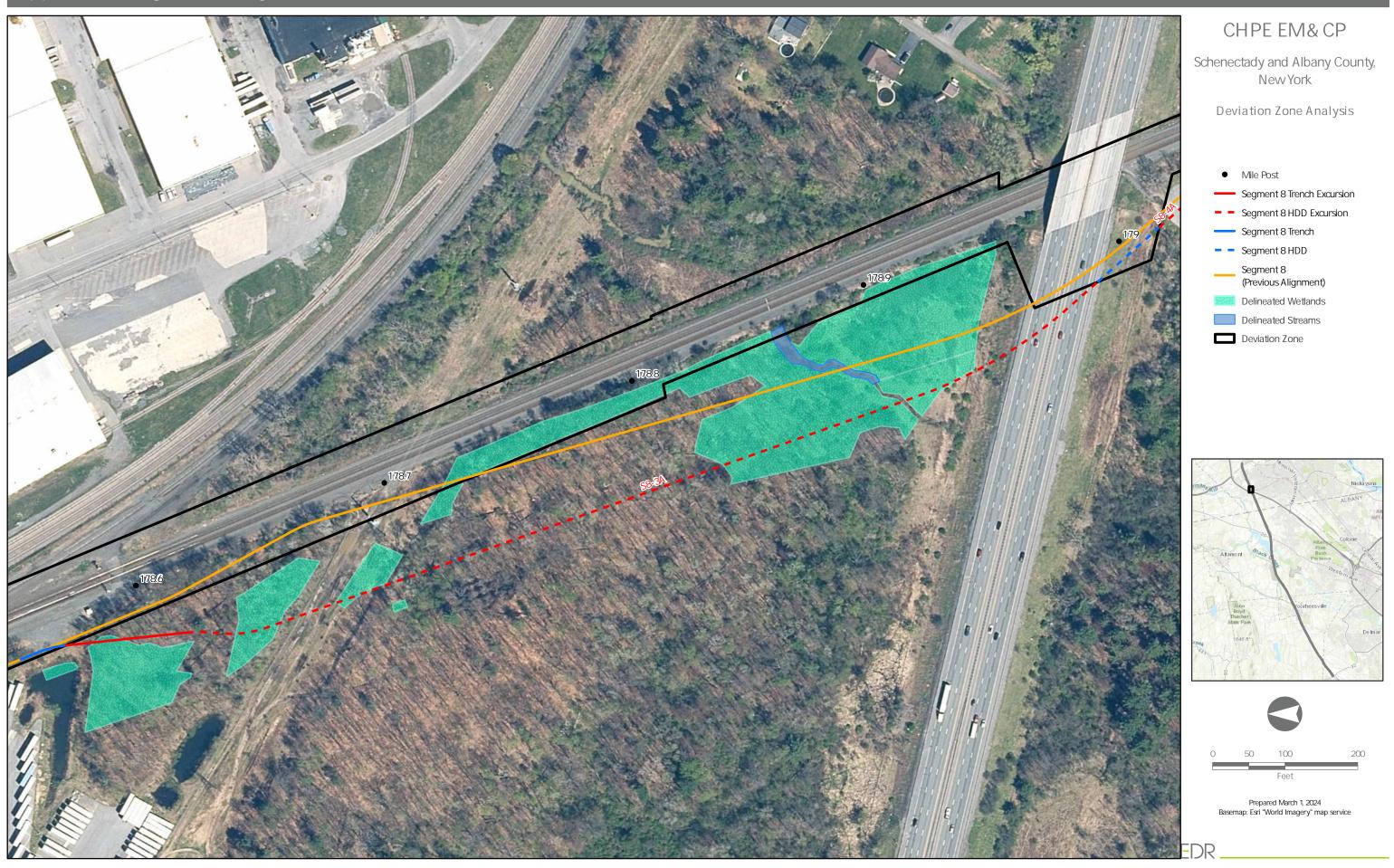




Segment 8 (Package 5A) **EM&CP Appendix E New Sheets**





Schenectady and Albany County,







Segment 8 (Package 5A) **EM&CP Appendix J Memo**



April 1, 2024 File No. 322004-000

Kiewit Engineering (NY) Corporation 470 Chestnut Ridge Rd, 2nd Floor Woodcliff Lake, NJ 07677

Attention: Jason Neff, PE, PMP - Design Engineering Manager

Subject: HDD 73A,74 Design Revisions

Champlain Hudson Power Express – Segment 5b

Rotterdam to Fuera Bush, NY

Dear Mr. Neff:

At your request, we have modified HDD 73A,74 to accommodate minor alignment modifications. Specifically, these modifications include reversal of the drilling direction and shifting of the HDD entry and exit pits. Amended text and design calculations are attached. The following is noted:

- The duct pull forces have not changed significantly; and
- The risk of IR increases at the drill exit, as the revised geometry involves drilling downslope. The driller will also need to be prepared to contain the drill fluid which will flow downhill to the exit pit during drilling.

The discussions and recommendations contained in the IFC HDD Basis of Design Report and IRR plan otherwise remain unchanged.

We thank you for this opportunity to be of service to you and your team on this project. Should you have any questions or require additional information, please do not hesitate to contact the undersigned at your convenience.

Sincerely,

Brierley Associates Underground Engineers, PLLC

Nick Strater, P.G.

Much Other

Trenchless Design Manager

Brian C. Dorwart, P.E., P.G.

But of

Sr. Consultant

1.0 Introduction

Table 1: HDD Locations, Lengths, and Description

HDD #	Approx. Start Station*	Approx. End Station*	Approx. HDD Length,	Obstruction Crossed
73A,74	50100+00	50120+04	2,004	NYS Throughway (I-90)

^{*}Project stationing shown is approximate. Each HDD has its own independent stationing.

4.1 Surface Conditions

HDD #73A,74

HDD #73A,74 pass below an overhead electric cable easement (Niagara Mohawk) which is oriented approximately northwest-south, and about 100-ft wide. Power poles are located to the west of the HDD alignments.

The HDD #73A,74 alignments also pass below Interstate I-90 which is oriented approximately southeast-northwest, 115-ft wide, and located on an elevated embankment. Interstate I-90 passes over two (2) active CSX rails to the immediate east by means of a concrete deck bridge. The western bridge abutment is located to the immediate east of the HDD alignments. The areas to the north of I-90 and adjacent to Niagara Mohawk easements are heavily wooded.

The HDD #73A,74 exit (southeast) is located in a paved cul-de-sac at the northeast end of S Westcott Rd. The HDD #73A,74 entry (northwest) is located in a wooded area to the northwest of the Niagara Mohawk easement. The CSX rails are located approximately at-grade to the east-northeast, and are oriented northwest-southeast. The CSX rails rest on an elevated embankment which is approximately 4 to 5 feet higher than adjacent grades. Portions of the HDD #73A,74 alignments are located within the CSX right-of-way.

The surface grades in the site vicinity generally slope downward to the south, from about El. 326 to El. 314. The surface of I-90 is at about El. 350.



APPENDIX BHDD Calculations Per Crossing



HORIZONTAL DIRECTIONAL DRILL DESIGN

PROJECT: Champlain Hudson Power Express

Segment 8 (Pkg. 5A) - CSX: Roterdam to Bethlehem

Schenectady County, NY

CROSSING: HDD 73A-74 Conduit #1

NY State Thruway(I-90)

ISSUE: Issued for Construction (IFC)

Contents:

Table 1	DESIGN SUMMARY, ASSUMPTIONS, CONDITIONS
Table 2	DRILL PATH DESIGN CALCULATIONS
Table 3	ANTICIPATED PULLING FORCE - SINGLE CONDUIT
Table 4	PLASTIC STRESS
Figure 1	APC AND FPC CURVES AND ASSUMED GEOLOGIC SECTION

Prepared For: Kiewit

Prepared By: Brierley Associates

167 S. River Road, Suite 8

Bedford, NH 03110 603.206.5775 (O)

Project No: 322004-000 Print Date: 1-Apr-2024



DATE	REV	DESCRIPTION	BY
10/23/2022	0	Design Submittal	ABL
3/23/2023	1	Issued for Construction	ABL
8/29/2023	2	Profile Revisions	KRF
3?31/24	3	Plan Revisions	NHS

DRILL PATH DESIGN CALCULATIONS Entry Station 0+00.00 Exit Station 20+45.21 FT

If no water or mudline then use lower of entry or exit elevation Water Surface Elev. 310.00 f Mudline Elev.* 310.00 f 273.60 f Lowest centerline Elev.

Entry and Exit Design Coordinates & Elevations (Ft) (Note 2) Elevation Fast North Entry 629021.1198 1437814.4763 326.40 ft 629520.3407 1436410.0486 Horizontal Curve PI 629890.9574 1435991.5954 Fxit 311.00 ft

Depth to Mudline 16.40 ft Clearance Depth = 36.40 ft Measured Plan Length at ties = 2045.2102 ft Coordinate Length = 2045.2102 ft OK-HORIZONTAL CURVE

		Start				End					
	Station	Easting	Northing	Station		Easting	Northing	Azimuth	Length	Radius	Angle
Tangent	0+00.00	629021.1198	1437814.4763		13+15.88	629461.8497	1436574.5977	E 160.43163 N	1315.88		
Curve	13+15.88	629461.8497	1436574.5977		16+60.86	629636.1280	1436279.3164	E 138.46925 N	344.98	900.00	-21.962 de
Tangent	16+60.86	629636.1280	1436279.3164		20+45.21	629890.9574	1435991.5954	E 138.46925 N	384.35		

SUMMARY HORIZONTAL CURVE CALCULATIONS

HORIZONTAL PLAN CALCULATIONS (FT)										Pull Geome	try			
Entry Tangent Segment		Horizontal Curve Seg	ment	Exit Tangent Segme	nt		Pipe Entry	Exit	Enter the pipe er	ntry location into the	hole: Entry/Exit			
Plan Length, ft.	1315.88	Input Radius, ft.	900.00	Plan Length, ft.	384.35			Elevat	ions	,	/ertical Angle		Path	Curve
Entry Azimuth, deg. ⁵ N	I 160.43163 E	Curve, deg	-21.962 deg.	Exit Azimuth, deg.5	N 138.46925 E		Segment	Start	End	Start	End	∆ Angle	Length	Radius
Entry Azimuth, rad. ⁵	2.80006	Curve, rad	-0.38332	Exit Azimuth, rad.5	2.41674		Entry Tangent	311.00 ft	291.47 ft	-9.90 deg	-9.90 deg	0.00 deg	113.60 ft	0.00 ft
		Calculate PTH		Calculate Exit			Entry Curve	291.47 ft	273.60 ft	-9.90 deg	0.00 deg	9.90 deg	207.35 ft	1200.00 ft
Calculate PCH		Chord Length, ft.	342.88	Easting	629890.9574	Check	Bottom Tangent	273.60 ft	273.60 ft	0.00 deg	0.00 deg	0.00 deg	1352.46 ft	0.00 ft
	629461.8497		344.98	Northing	1435991.5954	Delta	Exit Curve	273.60 ft	299.82 ft	0.00 deg	12.00 deg	12.00 deg	251.33 ft	1200.00 ft
PCH Northing 1	1436574.5977	Chord Azimuth, deg	149.4504			0.0000	Exit Tangent	299.82 ft	326.40 ft	12.00 deg	12.00 deg	0.00 deg	127.83 ft	0.00 ft
		PI Easting =	629520.3407			0.0000						Total Check =	2052.56 ft	OK
		PI Northing =	1436410.0486			OK CALC		Compound Curve A	Assessment					
		PTH Easting =	629636.1280					Star	Vert. Plan	Horiz. Plan				

374.53 1315.88 PTH Northing = 1436279.3164 **Exit Station** Entry No, Horiz > Entry V(Tan+Curve) 20+45.21 Exit 384.35 No, Horiz > Entry V(Tan+Curve) Cum Plan Length 1315.88 Cum Plan Length 1660.86 Cum Plan Length 2045.210223 OK STA

VERTICLE PATH	1 DESIGI	N CALCULAT	IONS (FT)								Summary of Dril
Entry Tangent Segment 1		Entry Vert. Curve Seg	gment 2	Middle Tangent Seg	ment 3	Exit Vert. Curve Segme	nt 4	Exit Tangent Segmen	t 5		Entry to E
Entry Angle	-12.000 deg.	Vertical Radius	1200.00	End Vert Angle	0.000 deg	Radius	1200.00	Exit Elevation	311.00		Minim
	_	Vert. Curve, deg.	12.000 deg	Inclined Bottom Tan	NO	Angle Change	9.900 deg.	Design Exit Angle	9.90 deg		In
											Inv
Calculate Vertical PCV		Calculate Vertical PT	V	Calculate Vertical P	CV	Calculate Vertical PTV		Calculate Exit		SUMS	
Plan Length	125.036 ft	Plan Length	249.494 f	Plan Length	1,352.45707 f	Plan Length	206.315 ft	Plan Length	111.909 ft	2,045.210 ft	
Rod Length	127.829 ft	Arc Rod Length	251.327 f	Rod Length	1,352.45707 f	Arc Rod Length	207.345 ft	Rod Length	113.600 ft	2,052.559 ft	Minimum Plan
Vertical Depth	-26.577 ft	Curve ∆ Vert Depth	-26.223 f	t Vertical Depth	0.00000 f	Curve ∆ Vert Depth	17.869 ft	Vertical Depth	19.531 ft	-15.400 ft	
		Lowest Elevation	273.600 f			Lowest Elevation	273.600 ft	CK Total Cum Depth	-15.400 ft		
Start Elevation	326.400 ft		299.823 f		273,600 f		273.600 ft		291,469 ft		Com
End Elevation	299.823 ft		273.600 f		273.600 f		291.469 ft				Coi
End Vert Angle	-12.000 deg	End Vert Angle	0.000 deg	End Vert Angle	0.000 deg	End Vert Angle	9.900 deg	Prop. Plan Length	2045.210223		<u> </u>
SUMMARY VERTICLE CUI	RVE CALCULA	ATIONS								Stationi	ng Check
Start Station	0+00.00	Start Station	1+25.04	Start Station	3+74.53	Start Station	17+26.99	Start Station	19+33.30	OK STA	ATIONING
PVC Station	1+25.04	PTV Station	3+74.53	PCV Station	17+26.99	PTV Station	19+33.30	Exit Station	20+45.210	Plan Len	gth Check
Cum Plan Length	125.04	Cum Plan Length	374.53	Cum Plan Length	1726.99 f	Cum Plan Length	1933.30	Cum Plan Length	2045.21	OK CAL	CULATION
Cum Rod Length	127.83	Cum Rod Length	379.16	Cum Rod Length	1731.61 f	Cum Rod Length	1938.96	Cum Rod Length	2052.56	Elevation C	hange Check
Cum Depth	-26.58	Cum Depth	-52.80	Cum Depth	-52.80 f	Cum Depth	-34.9312	Cum Depth	-15.40	OK CAL	CULATION

Summary of Drill Calculations Exit Elevation Change = -15.40 ft imum Design Elevation = 273.60 ft Invert Depth below exit = 37.40 ft nvert Depth below entry = 52.80 ft Path Length = 2,052.56 ft Plan Length = 2,045.21 ft an Length (No Tangent) = 692.75 ft Entry Angle = -12.00 deg Exit Angle = 9.90 deg mpound Curve at Entry = NO compound Curve at Exit =

NO

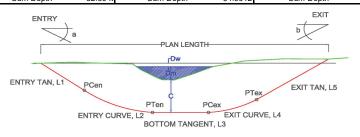
•
Stationing Check
OK STATIONING
Plan Length Check
OK CALCULATION
Elevation Change Check
OK CALCULATION

. Sign convention for angles - positive (+) angles are counterclockwise. Due East is defined as 0 degrees.

. NAD83 New York State Plane East Zone

3. Elevations are referenced to NAVD88 Datum

4. All calculation locations represent the center of the drill hole.



Indicates inputs Indicates status on internal design checks Issued for Construction (IFC)

BRIERLEY ASSOCIATES

ISSUE:

Champlain Hudson Power Express Segment 8 (Pkg. 5A) - CSX: Roterdam to Bethlehem Schenectady County, NY

TABLE 2

DRILL PATH DESIGN CALCULATION HDD 73A-74 Conduit #1 NY State Thruway(I-90) Brierley Associates

167 S. River Road, Suite 8 Bedford, NH 03110 Revision 3

TBD

Pull Geometry

Lengths (Path)			Angles				
L1 =	100.0 ft	Overbend	deg	radian	300.0 ft		
L2 =	113.6 ft	α =	-9.9 °	-0.1728			
L3 =	207.3 ft				1,200.0 ft		
L4 =	1352.5 ft	χ =	0.0 °	0.0000			
L5 =	251.3 ft				1,200.0 ft		
L6 =	127.8 ft	β =	12.0 °	0.2094			
LT =	2152.6 ft						

INPUT: Assumed Friction Factors

μ_G =	0.10	dry + rollers
μ_b =	0.25	drill fluid in hole
$\mu_c =$	0.30	in hole no fluid

INPUT: Assumed Hydrokinetic Drag

 $\tau_f = 0.005 \text{ psi}$ Drill Fluid Shear Stress

INPUT: Pipe Properties

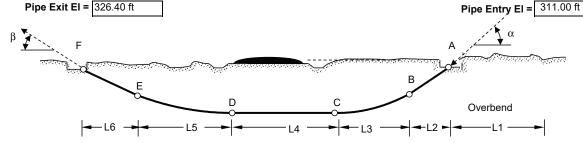
live o i . Fipe Fio	pernes	
Material	HDPE	IPS
Safe Pull Max. Stress, σ_{PM}	1,150 psi	PPI Table 1 12hr @ 73Deg F
Pile/Bundle Diam. 14.25	BUNDLE	PIPE/BUNDLE
Material Density, γ	59.28 pcf	
Outside Diameter, D _{OD}	14.25	Pipe or Bundle
Pipe Dry Weight, W _P =	17.36 lb/ft	Pipe or Bundle
Min. Wall Thickness, t _m	1.194 in	For design installation pull stress
$DR = D_O/t_{min} =$	9	D _{OD} Stress 10.75 inches
Avg. Inside Diameter, D _{IA}	BUNDLE	Bundle Multiplier F _D 0.9042
12 Hr Pullback Modulus, E _T =	65,000 psi	@T = 73 deg F
Poisson Ratio, μ =	0.45	
Ovality Factor, f _o =	0.84	2%
Buckling Safety, N =	2.5	
Hydrostatic Design Stress, HDS =	1,000 psi	HDB/2
Pressure Rating, PR _(80F) =	250 psi	$PR = 2HDSF_{T}A_{F}/(DR-1)[F_{T}=1]$
INPUT: Assume	d Fluid Dens	ities/Elevations

cf

•		
Ballast Density	62.4	pcf
Drill Fluid Density	78	pcf
Drill fluid elevation, H _F =	310.00 ft	
Ballast Water El., H _W =	310.00 ft	
Lowest Invert EI., $EI_m =$	273.60 ft	

Pipe Entry Location - Drill

(schematic, to show definition of variables only)



Exit

Calculated Pull Force								ASSESS	
POINT	Pull Force, F _D	Max Tensile	ASSESS	Pull Force, F _B	Max Tensile	ASSESS	F _x <	SPS	
FOINT	No Ballast	Stress, σ_T	$\sigma_{T} < \sigma_{PM}$	Ballasted Pipe	Stress, σ_T	$\sigma_T < \sigma_{PM}$	Air	Ballast	
Α	3,802 lb	225 psi	OK	3,802 lb	225 psi	OK	OK	OK	
В	4,689 lb	118 psi	OK	4,893 lb	123 psi	OK	OK	OK	
С	6,413 lb	194 psi	OK	5,729 lb	177 psi	OK	OK	OK	
D	12,688 lb	320 psi	OK	12,004 lb	303 psi	OK	OK	OK	
E	18,031 lb	487 psi	OK	14,932 lb	409 psi	OK	OK	OK	
F	19,348 lb	488 psi	OK	15,686 lb	396 psi	OK	OK	OK	
ASSESS P	ull Restricted Bu	uckling Capac	ity, P _{PA} > ∆P invert	$P_{PA} = P_A F_R =$	93.96 psi	Balla	sted	OK	

Maximum tensile stress during pullback = $\sigma_t = (F_T/\pi t_m(D_{OD}-t_m))+E_TD_{OD}/2R$

No Ballast PPI Ch 12 Eq 16 OK

Calculated Material Design Limits For Designed Drill Path

 $SSPS = \sigma_{PM} \pi D_{OD}^{2} ((1/DR) - (1/DR^{2}))$ Safe Pull Strength, SPS = 45,606 lb Allowable Short Term Unconstrained Buckling, PA = $P_A = (2E_T/(1-\mu^2))(1/(DR-1))^3(f_0/N)$ 106.97 psi 0.878323851 F_R = $(5.57-(r+1.09)^2)^{1/2}-1.09$ Maximum 12 hour Pull Stress Reduction, F_R = 0.21219093 $r = \sigma_T/2SPS$ Maximum applied pull Stress, σ_T = 488 psi From Pull Force Calculations Ballasted Max. Differential Pressure on Pipe, ΔP_B invert = 3.94 psi (-) indicates pipe is pressurized Unballasted Max. Differential Pressure on Pipe, ΔP_{II} invert = 19.72 psi (-) indicates pipe is pressurized

Calculated Drill Hole Diameter Assumed for Calculations

 D_0 <8" Use D_H = D_0 +4"; 8"< D_0 <24" Use D_H =1.5* D_0 ; D_0 >24" Use D_H = D_0 +12"

Calculated Pipe and Fluid Properties

Pressure Pipe:	YES	
OD Perimeter Length, P	44.77 in	
Wall Section Area, A _W	41.68747289	
Volume Outside, V_{DO}	0.697 cf/LF	
Volume Inside, V _{DI}	0.408 cf/LF	
$q_d =$	2.69 lb/ft	Drill Fluid (unit drag)
EQ 18: Hydrokinetic, $\Delta T =$	0.43 lb/ft	Comparison Only @ 8psi

Estimated for pull

Calculated Buoyant Forces

ASTM

	Pipe	Air Filled	Ballasted
	und, w _a /w _{af} =		42.80 Lb/LF
In Hole with Drill F	Fluid, $w_b/w_{bf} =$	-37.01 Lb/LF	-11.58 Lb/LF

NOTES: 1 - Calculations were done in general accordance with ASTMF-1962 as modified to account for invert tangent section, independent vertical curves, and fluid drag. ASTM applies hydrokinetic pressure as shear per unit pipe length requiring a back calculation to determine actual pull force based on average pipe area.

ISSUE: Issued for Construction (IFC)

BRIERLEY ASSOCIATES Limited Liability Company

Champlain Hudson Power Express

Segment 8 (Pkg. 5A) - CSX: Roterdam to Bethlehem

Schenectady County, NY

"Creating Space Underground"

TABLE 3 - PULL ASSESSMENT ANTICIPATED PULLING FORCE - HDPE PULL HDD 73A-74 Conduit #1

Brierley Associates 167 S. River Road, Suite 8 Bedford, NH 03110

Revision 3

NY State Thruway(I-90)

TBD

HDPE PROPERTIES

Champlain Hudson Power Express

Segment 8 (Pkg. 5A) - CSX: Roterdam to Bethlehem

Pg 1 of 3

Schenectady County, NY

HDD 73A-74 Conduit #1 NY State Thruway(I-90) BRIERLEY
ASSOCIATES
Limited Liability Company

"Creating Space Underground"

INPUTS

Pipe Material Properties

Sources: ASTM D3350 and Plastic Pipe Institute Publications and as referenced

Design Working Pressure, P _{WORK} Quantity of Pipes in Hole, Q = Pipe Material ASTM D3350 Cell Classification Standard Dimension Pipe measurement standard DR = OD/Minimum Wall Outside Diameter, D ₁ = 8.219 in Minimum Wall, t _{min} Wall Section Area, A _W = 1.194 in Unit OD Surface Area, in°/LF, A _{OD} = Unit Inside Volume, V _{D0} = Unit Inside Volume, V _{D0} = Design Factor for HDB, DF = Design Stress, HDS = Load Duration Duration Time Design Temperature, P _S = 3.500 psi Design Temperature, P _S = 1.500 psi NPUT RESIN MATERIAL: PE3408, PE3608, PE4710 Design resin with minimum PENT test of 10,000 hours Standard Manufacturer's Data Sheets	Sources. AS TW DSSSO	and Flastic Fip	e monute rubiic	alloris and as reference	u			
Pipe Material ASTM D3350 Cell Classification Standard Dimension 10 10 10 10 10 10 10 1	Design Working Pressure, P _{WORK}	250 psi		Test Pressure, P _{TEST}	0 psig	At high point		
ASTM D3350 Cell Classification Standard Dimension Pipe measurement standard DR = OD/Minimum Wall Outside Diameter, D, EAG = Avg. Inside Diameter, D, EAG =	Quantity of Pipes in Hole, Q =	1		•				
Standard Dimension Pipe measurement standard DR = OD/Minimum Wall Outside Diameter, D _o = 10.750 in Avg. Inside Diameter, D _o = 8.219 in Minimum Wall, t _{min} = 1.194 in Wall Section Area, A _W = 1.194 in Unit OD Surface Area, in '/LF, A _{OD} = 0.630 cf/LF Unit Inside Volume, V _{Do} = 0.630 cf/LF Unit Inside Volume, V _{Do} = 1.600 psi Environmental Factor, Af _e = 1.000 psi Environmental Factor, Af _e = 1.000 psi Density = 1.688 Lb/LF Tensile Yield, Ty psi = Load Duration Duration Time Design Temperature, °F Design Temperature, °F Design Ovality, % Factor of Safety, FS = 2.5 Modulus for given load duration, E = 65,000 psi Pipe Manufacturer's Data Sheets Standard Manufactu	Pipe Material	PE4710	INPUT RESIN M	MATERIAL: PE3408, PE	3608, PE47	10		
Pipe measurement standard DR = OD/Minimum Wall Outside Diameter, D ₀ = 10.750 in Avg. Inside Diameter, D ₁ = 8.219 in Minimum Wall, t _{min} = 1.194 in Wall Section Area, in 'f /LF, A _{OD} = 1.600 psi Unit OD Surface Area, in 'f /LF, A _{OD} = 0.630 cf/LF Unit OD surface Volume, V _{Di} = 0.630 cf/LF Unit OD surface Area, in 'f /LF, A _{OD} = 0.625 Unit OD surface Area, in 'f /LF, A _{OD} = 0.625 Unit OD surface Area, in 'f /LF, A _{OD} = 0.625 Unit OD surface Area, in 'f /LF, A _{OD} = 0.625 Unit OD surface Area, in 'f /LF, A _{OD} = 0.625 Unit OD surface Area, in 'f /LF, A _{OD} = 0.625 Unit OD surface Area, in 'f /LF, A _{OD} = 0.625 Unit OD surface Area, in 'f /LF, A _{OD} = 0.625 Unit OD surface Area, in 'f /LF, A _{OD} = 0.625 U	ASTM D3350 Cell Classification	445574C	Design resin with	h minimum PENT test of	f 10,000 hoເ	ırs		
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	Standard Dimension	10						
Outside Diameter, $D_o = Avg$. Inside Diameter, $D_i = Avg$. Insi	Pipe measurement standard	IPS	IPS "Iron Pipe S	ize" of DIPS "Ductile Iron	n Pipe Size'	•		
Avg. Inside Diameter, P_{i} = 8.219 in Minimum Wall, t_{min} = Wall Section Area, A_{W} = 1.194 in 35.85681985 $A_{W} = \pi^*(D_{o}/2 ^2 - (D_{o}-2t /2)^2 ^2)$ Unit OD Surface Area, in f/LF , A_{OD} = Unit Outside Volume, V_{Do} = Unit Inside Volume, V_{Do} = $0.630 \text{ cf}/LF$ $V_{Do} = \pi^*(D_{o}/2 ^2)^2/144$ $A_{OD} = 12^*\pi^*D_{OD}$ $A_{OD} = 1$	DR = OD/Minimum Wall	9						
Minimum Wall, t_{min} 3.194 in Wall Section Area, A_W 35.85681985 $A_W = \pi^*((D_o/2)^2 - ((D_o-2t)/2)^2)$ $A_{OD} = 12^*\pi^*D_{OD}$ $A_{OD} = 12^*T^*D_{OD}$ $A_{OD} = $	Outside Diameter, D _o =	10.750 in	Standard Manuf	acturer's Data Sheets				
$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	Avg. Inside Diameter, D _i =	8.219 in	Standard Manuf	acturer's Data Sheets				
Unit OD Surface Area, in $^{\prime}$ /LF, $A_{OD} = 0.630 \text{ cf/LF}$ $V_{Do} = \pi^{\star}(D_o/2)^2/144$ Unit Inside Volume, $V_{Do} = 0.630 \text{ cf/LF}$ $V_{Do} = \pi^{\star}(D_o/2)^2/144$ HDB = HDB = 0.636 cf/LF $V_{Di} = \pi^{\star}(D_o/2)^2/144$ Based on PPI Publication TR-4/2015 and ASTM 2837 Design Factor for HDB, DF = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 Hydrostatic Design Stress, HDS = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 HDB *DF Environmental Factor, Af_e = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 HDB *DF Environmental Factor, Af_e = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 HDB *DF Environmental Factor, Af_e = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 HDB *DF Environmental Factor, Af_e = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 HDB *DF Environmental Factor, Af_e = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 HDB *DF Environmental Factor, Af_e = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 HDB *DF Environmental Factor, Af_e = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 HDB *DF Environmental Factor, Af_e = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 HDB *DF Environmental Factor, Af_e = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 HDB *DF Environmental Factor, Af_e = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 HDB *DF Environmental Factor, Af_e = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 HDB *DF Environmental Factor, Af_e = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 HDB *DF Environmental Factor, Af_e = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 HDB *DF Environmental Factor, Af_e = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 HDB *DF Environmental Factor, Af_e = 0.625 Based on PPI Publication TR-4/2015 and ASTM 2837 Assumed Sactor PPI	Minimum Wall, t _{min} =	1.194 in	Standard Manuf	Standard Manufacturer's Data Sheets				
Unit Outside Volume, $V_{Do} = 0.630 \text{ cf/LF}$ $V_{Do} = \pi^*(D_o/2)^2/144$ Unit Inside Volume, $V_{Di} = 0.368 \text{ cf/LF}$ $V_{Di} = \pi^*(D_o/2)^2/144$ HDB = 1.600 psi Based on PPI Publication TR-4/2015 and ASTM 2837 Design Factor for HDB, DF = 0.625 Based on PPI PE Handbook 2nd ED Chapter 5 Hydrostatic Design Stress, HDS = 1000 psi HDS = HDB*DF Environmental Factor, $Af_e = 1$ Reference 2: Use for pressure rating only Density = 1000 psi HDS = HDB*DF Average from WL Plastics WL122 for PE4710 Weight Dry, W = 15.68 Lb/LF Tensile Yield, Ty psi = 1000 psi Gyrs Assumed Short Term Long Term Duration Time Duration Time Design Temperature, 9000 F To Besign Ovality, 9000 F To Besign Ovality, 9000 F To Gyrs Assumed See Sheets 4 of 5 for design ovality Factor of Safety, FS = 10000 Psi Based on PPI Handbook Ch. 3 and WL Plastics WL118-0314 Poisson Ratio, 9000 Psi Design Ovality factor 90000 Psi Design Ovality factor $9000000000000000000000000000000000000$	Wall Section Area, A _W =	35.85681985	$A_W = \pi^* ((D_o/2)^2 - (D_o/2)^2)$	$((D_o-2t)/2)^2)$				
Unit Inside Volume, $V_{Di} = 0.368 \text{ cf/LF}$ $V_{Di} = \pi^*(D_i/2)^2/144$ HDB = 1,600 psi Design Factor for HDB, DF = 1000 psi Hydrostatic Design Stress, HDS = Environmental Factor, Af _e = 1	Unit OD Surface Area, in ² /LF, A _{OD} =	405.27 in^2/LF	$A_{OD} = 12*\pi*D_{OD}$					
HDB = 1,600 psi Based on PPI Publication TR-4/2015 and ASTM 2837 Design Factor for HDB, DF = 0.625 Hydrostatic Design Stress, HDS = Environmental Factor, Af _e = 1 Reference 2: Use for pressure rating only Density = 59.28 pcf 1.410 g/cc Average from WL Plastics WL122 for PE4710 Weight Dry, W = 15.68 Lb/LF Tensile Yield, Ty psi = 3,500 psi @73°F	Unit Outside Volume, V _{Do} =	0.630 cf/LF	$V_{Do} = \pi^* (D_o/2)^2 / 1$	144				
Design Factor for HDB, DF = Hydrostatic Design Stress, HDS = $1000 \mathrm{psi}$ HDS = HDB*DF Environmental Factor, Af _e = Density = $1000 \mathrm{psi}$ HDS = HDB*DF Environmental Factor, Af _e = $1000 \mathrm{psi}$ HDS = HDB*DF Environmental Factor, Af _e = $1000 \mathrm{psi}$ Reference 2: Use for pressure rating only Average from WL Plastics WL122 for PE4710 Weight Dry, W = $15.68 \mathrm{Lb/LF}$ Tensile Yield, Ty psi = $1000 \mathrm{psi}$ Load Duration Duration Time $1000 \mathrm{hours}$ Short Term Long Term Duration Time $1000 \mathrm{hours}$ Short Term Long Term Design Temperature, °F $1000 \mathrm{psi}$ Assumed See Sheets 4 of 5 for design ovality Factor of Safety, FS = $1000 \mathrm{psi}$ Reference 2: Use for pressure rating only Average from WL Plastics WL122 for PE4710 Winimum from ASTM D3350 determined by ASTM D638 Short Term Long Term Assumed See Sheets 4 of 5 for design ovality Industry Practice Modulus for given load duration, E = $1000 \mathrm{mur}$ See Sheets 4 of 5 for design ovality Industry Practice Based on PPI Handbook Ch. 3 and WL Plastics WL118-0314 Poisson Ratio, $1000 \mathrm{mur}$ Poisson Ratio, $1000 \mathrm{mur}$ Reference 1: Based on Selected Design Ovality Temperature factor, $1000 \mathrm{mur}$ Reference 1: Based on Selected Design Ovality Source: WL Plastics WL118	Unit Inside Volume, V _{Di} =	0.368 cf/LF	$V_{Di} = \pi^* (D_i/2)^2/14$	44				
Hydrostatic Design Stress, HDS = 1000 psi HDS = HDB*DF Environmental Factor, Af _e = 1 Reference 2: Use for pressure rating only Density = 59.28 pcf 1.410 g/cc Average from WL Plastics WL122 for PE4710 Weight Dry, W = 15.68 Lb/LF Tensile Yield, Ty psi = 3,500 psi @73°F Load Duration Time Duration Time Design Temperature, °F Design Ovality, % Factor of Safety, FS = 2.5 2.5 Industry Practice Modulus for given load duration, E = 65,000 psi 28,000 psi Poisson Ratio, v = 0.45 0.45 Ovality factor f _o = 0.84 0.6 Reference 1: Based on Selected Design Ovality Temperature factor, f _t = 1.00 1.00 Source: WL Plastics WL118	HDB =	1,600 psi	Based on PPI P	ublication TR-4/2015 and	d ASTM 283	37		
Environmental Factor, Af _e = 1 Reference 2: Use for pressure rating only Density = 59.28 pcf 1.410 g/cc Weight Dry, W = 15.68 Lb/LF Tensile Yield, Ty psi = Load Duration Duration Time Duration Time Design Temperature, °F Design Ovality, % 2% 4% See Sheets 4 of 5 for design ovality Factor of Safety, FS = 2.5 2.5 Modulus for given load duration, E = 65,000 psi Ovality factor f _o = 0.84 0.6 Temperature factor, f _t = 1.00 1.00 Reference 2: Use for pressure rating only Average from WL Plastics WL122 for PE4710 Average from WL Plastics WL132 for DE4710 Average from WL Plas	Design Factor for HDB, DF =	0.625	Based on PPI P	E Handbook 2nd ED Ch	apter 5			
Density = 59.28 pcf 1.410 g/cc Weight Dry, W = 15.68 Lb/LF Tensile Yield, Ty psi = Load Duration Duration Time Design Temperature, °F Design Ovality, % Factor of Safety, FS = 2.5	Hydrostatic Design Stress, HDS =	1000 psi	HDS = HDB*DF					
Weight Dry, W = Tensile Yield, Ty psi = 3,500 psi @73°F Load Duration Duration Time Design Temperature, °F 73 deg F 73 deg F Design Ovality, % Factor of Safety, FS = 2.5 2.5 Industry Practice Modulus for given load duration, E = 65,000 psi Ovality factor f _o = 0.84 0.6 Reference 1: Based on Selected Design Ovality Source: WL Plastics WL118	Environmental Factor, Af _e =	1	Reference 2: Us	e for pressure rating only	у			
Tensile Yield, Ty psi = Load Duration Duration Time Design Temperature, °F Design Ovality, % Factor of Safety, FS = Modulus for given load duration, E = Ovality factor f _o = Ovality factor f _o = Ovality factor f _o = Temperature factor, f _t = 1.00 1.00 Source: WL Plastics WL118	Density =	59.28 pcf	1.410 g/cc A	Average from WL Plastic	s WL122 for	r PE4710		
Load Duration Duration Time Short Term Long Term Duration Time To hours 50 yrs Design Temperature, ${}^{\circ}F$ 73 deg F 73 deg F Design Ovality, ${}^{\circ}V$ 2% 4% See Sheets 4 of 5 for design ovality Industry Practice Modulus for given load duration, $E = 0.0000000000000000000000000000000000$	Weight Dry, W=	15.68	Lb/LF					
Duration Time Design Temperature, ${}^{\circ}F$ Design Ovality, ${}^{\circ}K$ Exactor of Safety, FS = 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5	Tensile Yield, Ty psi =	3,500 psi	@73°F	Minimum from ASTM D3	350 determi	ned by ASTM D638		
Design Temperature, ${}^{\circ}F$ Design Ovality, ${}^{\circ}$ Design Ovality, ${}^{\circ}$ Design Ovality, ${}^{\circ}$ Eactor of Safety, FS = 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5 2.5	Load Duration							
Design Ovality, % 2% 4% See Sheets 4 of 5 for design ovality 2% See Sheets 4 of 5 for design ovality Industry Practice Modulus for given load duration, E = $65,000 \text{psi}$ $28,000 \text{psi}$ Based on PPI Handbook Ch. 3 and WL Plastics WL118-0314 20% Poisson Ratio, 20% 20% 20% 20% WL118: Use 20% Use 20% 20% VWL118: Use 20% 20% Reference 1: Based on Selected Design Ovality 20% Temperature factor, 20% 20% 20% Source: WL Plastics WL118								
Factor of Safety, FS = $\frac{2.5}{65,000 \text{ psi}}$ Industry Practice Modulus for given load duration, E = $\frac{65,000 \text{ psi}}{65,000 \text{ psi}}$ 28,000 psi Based on PPI Handbook Ch. 3 and WL Plastics WL118-0314 Poisson Ratio, $v = \frac{0.45}{0.45}$ WL118: Use 0.35 if load duration is less than 12 hours Poisson Ratio, $v = \frac{0.84}{0.6}$ O.6 Reference 1: Based on Selected Design Ovality Temperature factor, $f_t = \frac{1.00}{1.00}$ Source: WL Plastics WL118	•		, o dog .					
Modulus for given load duration, E = $65,000 \text{ psi}$ $28,000 \text{ psi}$ Based on PPI Handbook Ch. 3 and WL Plastics WL118-0314 Poisson Ratio, $v = 0.45$ 0.45 WL118: Use 0.35 if load duration is less than 12 hours Reference 1: Based on Selected Design Ovality Temperature factor, $f_t = 1.00$ 1.00 Source: WL Plastics WL118	3,				sign ovality			
Poisson Ratio, $v = 0.45$ 0.45 WL118: Use 0.35 if load duration is less than 12 hours Ovality factor $f_0 = 0.84$ 0.6 Reference 1: Based on Selected Design Ovality Temperature factor, $f_t = 1.00$ 1.00 Source: WL Plastics WL118					0 114/1 5	N (') M (440 0044		
Ovality factor $f_0 = 0.84$	<u> </u>							
Temperature factor, f _t = 1.00 1.00 Source: WL Plastics WL118	·							
	_					sign Ovality		
Duciant Fluida		1.00	1.00	Source: WE Plastics WET	110			

Project Fluids

Pipe Internal Ballast	Ballast External Fluid				
Fresh Water	Drill Fluid 1	Drill Fluid 2			
γ_{INT}	$\gamma_{\sf EXT1}$	γ_{EXT2}			
62.4	78	80			
Density, $\gamma = 62.4$ 78 Buoyant Unballasted Fluid 1, B _{B1} =					
Buoyant Unballasted Fluid 2, B_{B2} =					
Ballasted or	n ground, $B_G =$	38.67 lb/ft			
nt Ballasted in F	Fluid 1, BB _{B1} =	-10.49 lb/ft			
nt Ballasted in	Fluid 2, $B_{BB2} =$	-11.75 lb/ft			
	Ballast Fresh Water γιντ 62.4 ant Unballasted ant Unballasted Ballasted on t Ballasted in F				

Dry Weight Pipe on ground, $W_P = 15.68 \text{ lb/ft}$ From MFG. Data Sheet Internal Ballast Weight, $W_B = 22.99 \text{ lb/ft}$ W_B = $V_{Di}^* \gamma_{INT}$ Expected Displaced Fluid Weight, $W_{D1} = 49.16 \text{ lb/ft}$ W_{D1} = $V_{Do}^* \gamma_{EXT1}$ Heavy Displaced Fluid Weight, $W_{D2} = 50.42 \text{ lb/ft}$ W_{D2} = $V_{Do}^* \gamma_{EXT2}$ W_P-W_{D1} W_P-W_{D2} W_P+W_B BG-W_{D1} BG-W_{D2}

Pg 2 of 3

HDPE PROPERTIES

Champlain Hudson Power Express

Segment 8 (Pkg. 5A) - CSX: Roterdam to Bethlehem

Schenectady County, NY

HDD 73A-74 Conduit #1

NY State Thruway(I-90)

1. ASSESS PIPE PRESSURE RATING

Failure mode: Short term = burst; Long term = slow crack growth

BRIERLEY
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Limited Liability Company

"Creating Space Underground"

Short Term (<10 hours)

Design Temperature, ${}^{\circ}F = 73 \text{ deg } F$ Ultimate Internal Pressure, $P_U = 875 \text{ psi}$ Allowable Internal Pressure, $P_A = 400 \text{ psi}$ $P_A = 2 * HDB * f_V (DR-1)$

ASSESSMENT TEST PRESSURE

OK OK if P_A >= to P_{TEST}

Long Term Design for operating conditions

Design Temperature, ${}^{\circ}F = \frac{73 \text{ deg F}}{Pressure \text{ Rating, PR}} = \frac{250 \text{ psi}}{PR} = 2*HDS*f_t*Af_e/(DR-1)$ Maximum Ocassional Surge, $P_{OS} = \frac{500 \text{ psi}}{375 \text{ psi}} = 1.5*PR$ Maximum Reoccuring Surge, PRS = $\frac{375 \text{ psi}}{P_{RS}} = 1.5*PR$

ASSESSMENT PRESSURE RATING
OK OK if PR >= to P_{WORK}

2. ASSESS PIPE UNCONSTRAINED BUCKLING CAPACITY FOR CONSTRUCTION PRESSURES

CALCULATE: Unconstrained Buckling Capacity of pipe

Unconstrained buckling ASTM F1962 EQ 5

Critical Pressure, $P_{CR} = f_o^*[2^*E/(1-v^2)]^*[(1/(DR-1))^3]$

	Short Term	Long Term
Design Temperature, F =	73 deg F	73 deg F
P _{CR} =	267.4 psi	82.3 psi
$P_a = P_{CR}/FS$	107.0 psi	32.9 psi

CALCULATE: internal and external pressure for deepest pipe invert depth and construction conditions

Critical unconstrained buckling pressure is at the pipe invert

Max. Depth to Invert 52.80 ft Ballast depth to invert, H_B

37.40 ft Drill Fluid depth to invert, H_{DF} 37.40 f

Pipe Invert Internal Pressure, P

 $\begin{array}{c|c} & \text{Air Ballast, P}_{A} & 0.00 \text{ psi} \\ \hline \text{Full Ballast, P}_{B} = \gamma_{\text{INT}}^{*} (H_{B} + D_{o}/24)/144 & 16.40 \text{ psi} \\ \end{array}$

Unconstrained buckling occurs when DIFFERENTIAL PRESSURE between the inside pressure plus pipe capacity is less than the outside pressure. $(P_1 + P_a) - P_E \le 0$

Differential Pressures	Short Term	Long Term	
Internal Air and External Fluid 1 = $(P_A + P_a) - P_{DF1}$	86.47 psi	12.41 psi	Pull Back Condition - Option 1
Internal Air and External Fluid 2 = $(P_A+P_a)-P_{DF2}$	85.95 psi	11.89 psi	Pull Back Condition - Option 2
Internal Ballasted and External Fluid 1 = $(P_B+P_a)-P_{DF1}$	102.87 psi	28.82 psi	Pull Back Condition - Option 3
Internal Ballasted and External Fluid 2 = $(P_B+P_a)-P_{DF2}$	102.35 psi	28.29 psi	Pull Back Condition - Option 4
Internal Ballasted and External Water = $(P_B+P_a)-P_W$	106.97 psi	32.92 psi	Long Term Operating Conditions
Internal Air and External Water = $(P_A+P_a)-P_W$	90.57 psi	16.51 psi	Operational Dewatering NO SOIL LOADS
·		•	_

ASSESSMENT UNCONSTRAINED BUCKLING ALONG DRILL PATH BY DIFFERENTIAL PRESSURE

Pipe installation pressure differential does not require ballasting the pipe during pull-back

Pipe may be fully dewatered for operational conditions providing there is no soil loading. Soil loads not assessed.

Engineer to assess any dewatering of the pipe in the future for stability based on actual project conditions and time duration.

1.CHBD14734 74 CID #1 ABC 20340331 428154

HDPE PROPERTIES

Champlain Hudson Power Express

Segment 8 (Pkg. 5A) - CSX: Roterdam to Bethlehem

Safe Pull Strength, SPS Pipe =

Schenectady County, NY

HDD 73A-74 Conduit #1

NY State Thruway(I-90)

3. ASSESS ULTIMATE PULL STRENGTH (UPS) AND SAFE PULL STRENGTH (SPS)

Pg 3 of 3

Source PPI PE Handbook Ch 12 Formula 17 SPS = $\pi^*DF^*(Ty)^*D_0^{2*}((1/DR)-(1/DR^2))$

Designed Pull Duration Time = 12 hr Quantity of pipes, Q = Yield Strength Factor, fy = 0.4 Pull Temperature, F = 73 deg. Recommended (FS = 2.5) Pull Time factor, $f_T =$ 1 Plexco Engineering Manual Table 3.7 Design Factor, DF = $f_T * f_Y$ SAFE PULL STRENTH, SPS = 0.4 50,200 lb Temperature factor, f_{temp} = Ultimate Pull Strength, UPS = 125,499 lb 1 Temp Corr Tensile Yield, Ty*f_{temp} = 3,500 psi $SAS = Ty*f_{temp}*DF$ Suggested SSAS = 1,150 psi Safe Allowable Stress, SAS = 1,400 psi

41,235 lb

Using SSAS =

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ASSOCIATES

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OK as >0

Short Term Critical Unconstrained Buckling Pcr reduced for pull tension, PcrR = Pcr*fr

50,200 lb

(ASTM F-1962 EQ. 22)

Pull Duration Time =	12 Hr	Pcr =	267.4 psi	
SAS =	1,400 psi	Design Depth in DF, H _{MDF} =	0.0 ft	
Estimated Maximum Pull Stress, σ_i =	1,150 psi	Design Assumption as Maximum		
fr = ((5.57-(r+1.09)^2)^.5)-1.09 =	0.87832			
$r = \sigma_i/2*(SSAS) =$	0.21219	Example froi	m Table T5, σ_i =	488 psi
$P_{CRR} =$	234.9 psi			
FS =	2.0			
$P_{ACRR} = P_{CRR}/FS =$	117.4 psi	Allowable Reduced Short Term Buck	kling pressure du	ring pull
Internal Ballasted and External Fluid 1 = (P _B +P _{ACRR})-P _{DF1}	96.95 psi Pull Back Condition	n - Option 3	OK as >0

Internal Ballasted and External Fluid 2 = (P_B+P_{ACRR})-P_{DF2} 96.42 psi Pull Back Condition - Option 4

ASSESSMENT OF SAFE PULL STRENGTH ON TENSION REDUCED BUCKLING CAPACITY

ACCEPTIBLE Acceptible if differential pressures > 0 for reduced buckling capacity

REFERENCE 1 - Plastic Pipe Institute - Handbook of PE Pipe 2nd Edition

REFERENCE 2 - Plastic Pipe Institute - Handbook of PE Pipe 2nd Edition

Design Factor (fe) to apply to HDB

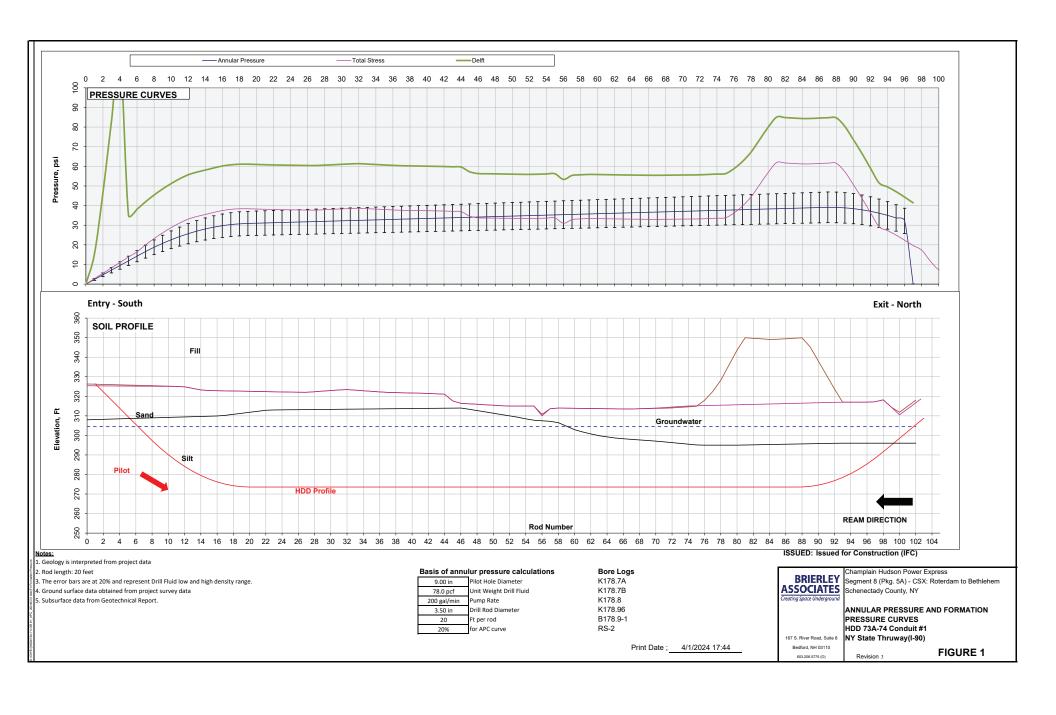
CHAPTER 6 - TABLE 1-2

REFERENCE 3 - Plexco Engineering Manual Book 3 Ch 3 Table 3.7

Time factor for pull duration, f_T

	f_T	Time factor for pull	
	1.00	Up to 1 hour pull	1
APCL	0.95	Up tp 12 hours pull	12
JF1A	0.91	Up to 24 hours	24

HPE\(HDD#73A-74 CIR #1_APC_20240331.xisb]F1A APCL





HORIZONTAL DIRECTIONAL DRILL DESIGN

PROJECT: Champlain Hudson Power Express

Segment 8 (Pkg. 5A) - CSX: Roterdam to Bethlehem

Schenectady County, NY

CROSSING: HDD 73A-74 Conduit #2

NY State Thruway (I-90)

ISSUE: Issued for Construction (IFC)

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Table 2	DRILL PATH DESIGNCALCULATIONS
Table 3	ANTICIPATED PULLING FORCE - CONSTANT FORCE
Table 4	PLASTIC STRESS
Figure 1	APC AND FPC CURVES AND ASSUMED GEOLOGIC SECTION

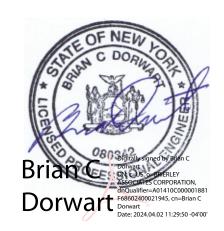
Prepared For: Kiewit

Prepared By: Brierley Associates

167 S. River Road, Suite 8

Bedford, NH 03110 603.206.5775 (O)

Project No: 322004-000 Print Date: 1-Apr-2024



Date	ID	DESCRIPTION	BY
10/23/2022	0	Design Submittal	ABL
3/23/2023	1	Issued for Construction	ABL
8/29/2023	2	Profile Alterations	KRF
4/1/2024	3	Plan Revision	NHS

DRILL PATH DESIGN CALCULATIONS Entry Station 0+00.00

Entry

Horizontal Curve PI

Exit Station

20+37.76 FT Entry and Exit Design Coordinates & Elevations (Ft) (Note 2) North Elevation East 629035.3157 1437819.6222 325.80 ft 1436408.1216 629546.9663 629902.4145 1436001.2771 311.30 ft

Exit Clearance Depth = Depth to Mudline 15.80 ft Measured Plan Length at ties = 2037.7571 ft ngth = 2037.7571 ft
OK-HORIZONTAL CURVE Coordinate Length =

If no water or mudline then use lower of entry or exit elevation Water Surface Elev. 310.00 ft Mudline Elev.3 310.00 ft Lowest centerline Elev. 273.80 ft

		Start				End					
	Station	Easting	Northing	Station		Easting	Northing	Azimuth	Length	Radius	Angle
Tangent	0+00.00	629035.3157	1437819.6222		13+32.80	629489.5177	1436566.6062	E 160.07508 N	1332.80		
Curve	13+32.80	629489.5177	1436566.6062		16+66.09	629657.8784	1436281.1720	E 138.85723 N	333.29	900.00	-21.218 deg.
Tangent	16+66.09	629657.8784	1436281.1720		20+37.76	629902.4145	1436001.2771	E 138.85723 N	371.67		_

SUMMARY HORIZONTAL CURVE CALCULATIONS

				LATIONS (F			_
Entry Tangent Segment		Horizontal Curve Seg		Exit Tangent Segme			L
Plan Length, ft.	1332.80	Input Radius, ft.	900.00	J ,	371.67		
Entry Azimuth, deg.5	N 160.07508 E	Curve, deg	-21.218 deg.	Exit Azimuth, deg.5	N 138.85723 E		
Entry Azimuth, rad.5	2.79384	Curve, rad	-0.37032	Exit Azimuth, rad.5	2.42352		Е
		Calculate PTH		Calculate Exit			Е
Calculate PCH	•	Chord Length, ft.	331.39	Easting	629902.4145	Check	В
PCH Easting	629489.5177		333.29		1436001.2771	Delta	Е
PCH Northing	1436566.6062	Chord Azimuth, deg	149.4662	-		0.0000	E
		PI Easting =	629546.9663			0.0000	46
		PI Northing =	1436408.1216			OK CALC	
		PTH Easting =	629657.8784				
		PTH Northing =	1436281.1720			Exit Station 20+37.76	
Cum Plan Length	1332.80	Cum Plan Length	1666.09	Cum Plan Length	2037.75707	OK STA	4

36.20 ft

	Pull Geometry							
	Pipe Entry Exit Enter the pipe entry location into the hole: Entry/Exit							
		Eleva	ations		Vertical Angle		Path	Curve
	Segment	Start	End	Start	End	∆ Angle	Length	Radius
E	Entry Tangent	311.30 ft	292.03 ft	-10.00 deg	-10.00 deg	0.00 deg	110.97 ft	0.00 ft
E	Entry Curve	292.03 ft	273.80 ft	-10.00 deg	0.00 deg	10.00 deg	209.44 ft	1200.00 ft
E	Bottom Tangent	273.80 ft	273.80 ft	0.00 deg	0.00 deg	0.00 deg	1349.33 ft	0.00 ft
E	Exit Curve	273.80 ft	300.02 ft	0.00 deg	12.00 deg	12.00 deg	251.33 ft	1200.00 ft
E	Exit Tangent	300.02 ft	325.80 ft	12.00 deg	12.00 deg	0.00 deg	123.98 ft	0.00 ft
	_	_	_			Total Check =	2045.05 ft	OK

Compound Curve Assessment

Start Vert. Plan Horiz. Plan 370.77 1332.80 Entry No, Horiz > Entry V(Tan+Curve) Exit 317.66 371.67 No, Horiz > Entry V(Tan+Curve)

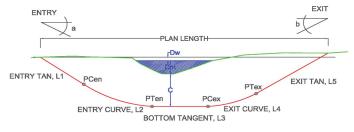
VERTICLE PATH DESIGN CALCULATIONS (FT)										
Entry Tangent Segment 1		Entry Vert. Curve Segm	ent 2	Middle Tangent Seg	ment 3	Exit Vert. Curve Segme	ent 4	Exit Tangent Segment 5		
Entry Angle	-12.000 deg.	Vertical Radius	1200.00	End Vert Angle	0.000 deg.	Radius	1200.00	Exit Elevation	311.30	
_	_	Vert. Curve, deg.	12.000 deg.	Inclined Bottom Tan	NO	Angle Change	10.000 deg.	Design Exit Angle	10.00 deg	
		0 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1								011140
Calculate Vertical PCV		Calculate Vertical PTV		Calculate Vertical P	CV	Calculate Vertical PTV		Calculate Exit		SUMS
Plan Length	121.272 ft	Plan Length	249.494 ft	Plan Length	1,349.33176 ft	Plan Length	208.378 ft	Plan Length	109.282 ft	2,037.757 ft
Rod Length	123.981 ft		251.327 ft	Rod Length	1,349.33176 ft		209.440 ft	Rod Length	110.967 ft	2,045.047 ft
Vertical Depth	-25.777 ft	Curve ∆ Vert Depth	-26.223 ft	Vertical Depth	0.00000 ft	Curve ∆ Vert Depth	18.231 ft	Vertical Depth	19.269 ft	-14.500 ft
		Lowest Elevation	273.800 ft			Lowest Elevation	273.800 ft	CK Total Cum Depth	-14.500 ft	
Start Elevation	325.800 ft	Start Elevation	300.023 ft	Start Elevation	273.800 ft	Start Elevation	273.800 ft	Start Elevation	292.031 ft	
End Elevation	300.023 ft	End Elevation	273.800 ft	End Elevation	273.800 ft	End Elevation	292.031 ft	Ck Exit Elevation		
End Vert Angle	-12.000 deg	End Vert Angle	0.000 deg	End Vert Angle	0.000 deg	End Vert Angle	10.000 deg	Prop. Plan Length	2037.75707	
SUMMARY VERTICLE CU	RVE CALCULA	ATIONS								Stationi
Start Station	0+00.00	Start Station	1+21.27	Start Station	3+70.77	Start Station	17+20.10	Start Station	19+28.48	OK STA
PVC Station	1+21.27	PTV Station	3+70.77	PCV Station	17+20.10	PTV Station	19+28.48	Exit Station	20+37.757	Plan Len

Summary of Drill Calculations	
Entry to Exit Elevation Change =	-14.50 ft
Minimum Design Elevation =	273.80 ft
Invert Depth below exit =	37.50 ft
Invert Depth below entry =	52.00 ft
Path Length =	2,045.05 ft
Plan Length =	2,037.76 ft
Minimum Plan Length (No Tangent) =	688.43 ft
Entry Angle =	-12.00 deg
Exit Angle =	10.00 deg
Compound Curve at Entry =	NO
Compound Curve at Exit =	NO

Start Elevation 620.000 it Start Elevation 600.020 it Start Elevation 270.000 it Start Elevation 200.020 it	0011
End Elevation 300.023 ft End Elevation 273.800 ft End Elevation 273.800 ft End Elevation 292.031 ft Ck Exit Elevation	Co
End Vert Angle -12.000 deg End Vert Angle 0.000 deg End Vert Angle 0.000 deg End Vert Angle 10.000 deg Prop. Plan Length 2037.75707	
UMMARY VERTICLE CURVE CALCULATIONS Statio	ning Check
Start Station 0+00.00 Start Station 1+21.27 Start Station 3+70.77 Start Station 17+20.10 Start Station 19+28.48 OK S	TATIONING
PVC Station 1+21.27 PTV Station 3+70.77 PCV Station 17+20.10 PTV Station 19+28.48 Exit Station 20+37.757 Plan L	ngth Check
Cum Plan Length 121.27 Cum Plan Length 370.77 Cum Plan Length 1720.10 ft Cum Plan Length 1928.48 Cum Plan Length 2037.76 OK CA	LCULATION
Cum Rod Length 123.98 Cum Rod Length 375.31 Cum Rod Length 1724.64 ft Cum Rod Length 1934.08 Cum Rod Length 2045.05 Elevation	Change Check
Cum Depth -25.78 Cum Depth -52.00 Cum Depth -52.00 ft Cum Depth -33.7693 Cum Depth -14.50 OK CA	LCULATION

- 1. Sign convention for angles positive (+) angles are counterclockwise. Due East is defined as 0 degrees. Due East is defined as a degree.

 2. NAD83 New York State Plane East Zone
- 3. Elevations are referenced to NAVD88 Datum
- 4. All calculation locations represent the center of the drill hole.



Indicates inputs Indicates status on internal design checks

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Champlain Hudson Power Express **BRIERLEY**

Segment 8 (Pkg. 5A) - CSX: Roterdam to Bethlehem **ASSOCIATES** Schenectady County, NY

DRILL PATH DESIGN CALCULATIONS

Bedford, NH 03110

HDD 73A-74 Conduit #2 NY State Thruway (I-90) Brierley Associates 167 S. River Road, Suite 8

> Revision 3 TBD

Pull Geometry

Lengths (Path)		Radius, R		
L1 = 100.0 ft	Overbend	deg	radian	300.0 ft
L2 = 111.0 ft	α =	-10.0 °	-0.1745	
L3 = 209.4 ft				1,200.0 ft
L4 = 1349.3 ft	χ =	0.0 °	0.0000	
L5 = 251.3 ft				1,200.0 ft
L6 = 124.0 ft	β =	12.0 °	0.2094	
LT = 2145.0 ft				

INPUT: Assumed Friction Factors

μ_G =	0.10	dry + rollers
$\mu_b =$	0.25	drill fluid in hole
$\mu_c =$	0.30	in hole no fluid

INPUT: Assumed Hydrokinetic Drag

0.005 psi Drill Fluid Shear Stress

INPUT:	Pipe Pro					
	Material	HDPE		IPS		
Safe Pull Max. S	Stress, σ_{PM}	1,150 psi	PPI Table 1	12hr @	73Deg F	
Pile/Bundle Diam.	10.75	PIPE	PIPE/BUND	LE		
Materia	l Density, γ	59.28 pcf				
Outside Dia	meter, D _{OD}	10.75	Pipe or Bun	dle		
Pipe Dry We	eight, W _P =	15.70 lb/ft	Pipe or Bun	Pipe or Bundle		
Min. Wall Th	ickness, t _m	1.194 in	For design installation pull stress			
DR	$= D_O/t_{min} =$	9	D _{OD} Stress	10.75	inches	
Avg. Inside Dia	ameter, D _{IA}	8.22 in	Bundle Mult	tiplier F _D	1.0000	
12 Hr Pullback Mod	dulus, E _T =	65,000 psi	@T =	73 deg F		
Poisson	Ratio, μ =	0.45		_		
Ovality I	actor, f _o =	0.84	2%			
Buckling S	Safety, N =	2.5		•'		
Hydrostatic Design St	ress, HDS =	1,000 psi	HDB/2			
Pressure Rating	g, PR _(80F) =	250 psi	PR = 2HDS	$SF_TA_F/(D$	R-1) [F _T =1]	
INPUT: Assumed Fluid Densities/Elevations						

62.4

78

310.00 ft

310.00 ft

273.80 ft

Calculated Pipe and Fluid Properties

Ballast Density

Drill Fluid Density

Drill fluid elevation, H_F =

Ballast Water El., H_w =

Lowest Invert El., El_m =

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Pressure Pipe:	YES	
OD Perimeter Length, P	33.77 in	
Wall Section Area, A _W	37.70738915	
Volume Outside, V _{DO}	0.630 cf/LF	
Volume Inside, V_{DI}	0.368 cf/LF	
$q_d =$	2.03 lb/ft	Drill Fluid (unit drag)
ASTM EQ 18: Hydrokinetic, $\Delta T =$	0.32 lb/ft	Comparison Only @ 8psi

pcf

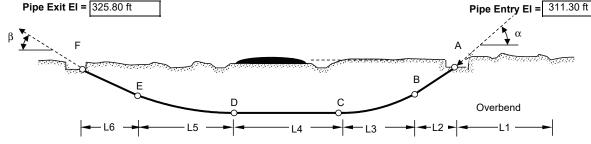
Estimated for pull

Calculated Buoyant Forces

•	Pipe	Air Filled	Ballasted
	und, w _a /w _{af} =		38.69 Lb/LF
In Hole with Drill F	Fluid, $w_b/w_{bf} =$	-33.46 Lb/LF	-10.47 Lb/LF

Pipe Entry Location - Drill

(schematic, to show definition of variables only)



Exit

	Calculated Pull Force							ASSESS	
POINT	Pull Force, F _D	Max Tensile	ASSESS	Pull Force, F _B	Max Tensile	ASSESS	F _x <	SPS	
FOINT	No Ballast	Stress, σ_T	$\sigma_{T} < \sigma_{PM}$	Ballasted Pipe	Stress, σ_T	$\sigma_T < \sigma_{PM}$	Air	Ballast	
Α	3,427 lb	193 psi	OK	3,427 lb	193 psi	OK	OK	OK	
В	4,257 lb	119 psi	OK	4,429 lb	124 psi	OK	OK	OK	
С	5,738 lb	184 psi	OK	5,104 lb	167 psi	OK	OK	OK	
D	11,404 lb	318 psi	OK	10,770 lb	300 psi	OK	OK	OK	
E	16,126 lb	474 psi	OK	13,307 lb	396 psi	OK	OK	OK	
F	17,269 lb	482 psi	OK	13,952 lb	389 psi	OK	OK	OK	
ASSESS	Pull Restricted	Buckling Cap	acity, P _{PA} > ∆P invert	$P_{PA} = P_A F_R =$	94.15 psi	Balla	sted	OK	

Maximum tensile stress during pullback = σ_t = $(F_T/\pi t_m(D_{OD}-t_m))+E_TD_{OD}/2R$

No Ballast PPI Ch 12 Eq 16 OK

Calculated Material Design Limits For Designed Drill Path

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Safe Pull Strength, SPS =	,	$SSPS = \sigma_{PM} \pi D_{OD}^{2} ((1/DR) - (1/DR^{2}))$
Allowable Short Term Unconstrained Buckling, P_A =	106.97 psi	$P_A = (2E_T/(1-\mu^2))(1/(DR-1))^3(f_o/N)$
Maximum 12 hour Pull Stress Reduction, F_R =	0.880121965	$F_R = (5.57 - (r + 1.09)^2)^{1/2} - 1.09$
r =	0.209468908	$r = \sigma_T/2SPS$
Maximum applied pull Stress, σ_T =	482 psi	From Pull Force Calculations
Ballasted Max. Differential Pressure on Pipe, ΔP_B invert =	3.92	psi (-) indicates pipe is pressurized
Unballasted Max. Differential Pressure on Pipe, ΔP_U invert =	19.61	psi (-) indicates pipe is pressurized

Calculated Drill Hole Diameter Assumed for Calculations

D_H =

 D_O <8" Use D_H = D_O +4"; 8"< D_O <24" Use D_H =1.5* D_O ; D_O >24" Use D_H = D_O +12"

NOTES: 1 - Calculations were done in general accordance with ASTMF-1962 as modified to account for invert tangent section, independent vertical curves, and fluid drag. ASTM applies hydrokinetic pressure as shear per unit pipe length requiring a back calculation to determine actual pull force based on average pipe area.

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Segment 8 (Pkg. 5A) - CSX: Roterdam to Bethlehem

Schenectady County, NY

TABLE 3 - PULL ASSESSMENT

ANTICIPATED PULLING FORCE - HDPE PULL

HDD 73A-74 Conduit #2 NY State Thruway (I-90) Brierley Associates

Bedford, NH 03110 Revision 3 TBD

HDPE PROPERTIES

Champlain Hudson Power Express

Segment 8 (Pkg. 5A) - CSX: Roterdam to Bethlehem

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Schenectady County, NY

HDD 73A-74 Conduit #2 NY State Thruway (I-90) ASSOCIATES
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INPUTS

Pipe Material Properties

Sources: ASTM D3350 and Plastic Pipe Institute Publications and as referenced

Design Working Pressure, P _{WORK}	250 psi		Test Pressure, P _{TEST} 0 psig At high point			
Quantity of Pipes in Hole, Q =	1					
Pipe Material	PE4710	INPUT RESIN	MATERIAL: PE3408, PE3608, PE4710			
ASTM D3350 Cell Classification	445574C	Design resin v	with minimum PENT test of 10,000 hours			
Standard Dimension	10					
Pipe measurement standard	IPS	IPS "Iron Pipe Size" of DIPS "Ductile Iron Pipe Size"				
DR = OD/Minimum Wall	9					
Outside Diameter, D_o =	10.750 in	Standard Mar	nufacturer's Data Sheets			
Avg. Inside Diameter, D _i =	8.219 in	Standard Mar	nufacturer's Data Sheets			
Minimum Wall, t_{min} =	1.194 in	Standard Mar	nufacturer's Data Sheets			
Wall Section Area, A _W =	35.85681985	$A_W = \pi^*((D_o/2))$	$(D_0-2t)/2$			
Unit OD Surface Area, in /LF, A _{OD} =	405.27 in^2/LF	$A_{OD} = 12^* \pi^* D_{OD}$				
Unit Outside Volume, V _{Do} =	0.630 cf/LF	$V_{Do} = \pi^* (D_o/2)^2 / 144$				
Unit Inside Volume, V _{Di} =	0.368 cf/LF	$V_{Di} = \pi^* (D_i/2)^2 / 144$				
HDB =	1,600 psi	Based on PPI Publication TR-4/2015 and ASTM 2837				
Design Factor for HDB, DF =	0.625	Based on PPI	PE Handbook 2nd ED Chapter 5			
Hydrostatic Design Stress, HDS =	1000 psi	HDS = HDB*[DF .			
Environmental Factor, Af _e =	1	Reference 2:	Use for pressure rating only			
Density =	59.28 pcf	1.410 g/cc	Average from WL Plastics WL122 for PE4710			
Weight Dry, W =	15.68	Lb/LF				
Tensile Yield, Ty psi =	3,500 psi	@73°F	Minimum from ASTM D3350 determined by ASTM D638			
Load Duration		Long Term				
Duration Time		50 yrs	<u>.</u>			
Design Temperature, °F	73 deg F	73 deg F	Assumed			
Design Ovality, %	2%	4%	See Sheets 4 of 5 for design ovality			
Factor of Safety, FS =	2.5	2.5	Industry Practice			
Modulus for given load duration, E =	65,000 psi	28,000 psi	Based on PPI Handbook Ch. 3 and WL Plastics WL118-0314			
Poisson Ratio, υ =	0.45	0.45	WL118: Use 0.35 if load duration is less than 12 hours			
Ovality factor f _o =	0.84	0.6	Reference 1: Based on Selected Design Ovality			
Temperature factor, $f_t =$	1.00	1.00	Source: WL Plastics WL118			

Project Fluids

	Pipe Internal Ballast	Expected External Fluid	Heavy External Fluid
Fluids	Fresh Water	Drill Fluid 1	Drill Fluid 2
	γ_{INT}	$\gamma_{\sf EXT1}$	$\gamma_{\sf EXT2}$
Density, γ =	62.4	78	80
Buoya	-33.48 lb/ft		
Buoya	-34.74 lb/ft		
	38.67 lb/ft		
Buoyar	-10.49 lb/ft		
Buoyant Ballasted in Fluid 2, B _{BB2} =			-11.75 lb/ft

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HDPE PROPERTIES

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Segment 8 (Pkg. 5A) - CSX: Roterdam to Bethlehem

Schenectady County, NY

HDD 73A-74 Conduit #2

NY State Thruway (I-90)

1. ASSESS PIPE PRESSURE RATING

Failure mode: Short term = burst; Long term = slow crack growth

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Short Term (<10 hours)

Design Temperature, ${}^{\circ}F = 73 \text{ deg } F$ Ultimate Internal Pressure, $P_U = 875 \text{ psi}$ Allowable Internal Pressure, $P_A = 400 \text{ psi}$ $P_U = 2*Ty*f_t/(DR-1)$ $P_A = 2*HDB*f_t/(DR-1)$

ASSESSMENT TEST PRESSURE

OK

OK if P_A >= to P_{TEST}

Long Term Design for operating conditions

Design Temperature, ${}^{\circ}F = 73 \text{ deg F}$ Pressure Rating, PR = 250 psiMaximum Ocassional Surge, P_{OS} = 500 psiMaximum Reoccuring Surge, PRS = 375 psiPR = $2*\text{HDS*f}_t*\text{Af}_e/(DR-1)$ P_{OS} = 2*PRP_{RS} = 1.5*PR

ASSESSMENT PRESSURE RATING
OK OK if PR >= to P_{WORK}

2. ASSESS PIPE UNCONSTRAINED BUCKLING CAPACITY FOR CONSTRUCTION PRESSURES

CALCULATE: Unconstrained Buckling Capacity of pipe

Unconstrained buckling ASTM F1962 EQ 5

Critical Pressure, $P_{CR} = f_0 * [2*E/(1-v^2)]*[(1/(DR-1))^3]$

Design Temperature, F = $\begin{bmatrix} Short Term \\ 73 deg F \end{bmatrix}$ $\begin{bmatrix} 73 deg F \\ P_{CR} \end{bmatrix}$ $\begin{bmatrix} 267.4 psi \\ P_{a} = P_{CR}/FS \end{bmatrix}$ $\begin{bmatrix} 267.4 psi \\ 107.0 psi \end{bmatrix}$ $\begin{bmatrix} 32.9 psi \\ 32.9 psi \end{bmatrix}$

CALCULATE: internal and external pressure for deepest pipe invert depth and construction conditions

Critical unconstrained buckling pressure is at the pipe invert

Max. Depth to Invert 52.00 ft Ballast depth to invert, H_B

37.50 ft Drill Fluid depth to invert, H_{DF} 37.50

Pipe Invert External Pressure, P_E

Pipe Invert Internal Pressure, P

 $\begin{array}{c|c} & \text{Air Ballast, P}_{A} & 0.00 \text{ psi} \\ \hline \text{Full Ballast, P}_{B} = \gamma_{\text{INT}}^{*} (H_{B} + D_{o}/24)/144 & 16.44 \text{ psi} \\ \end{array}$

Unconstrained buckling occurs when DIFFERENTIAL PRESSURE between the inside pressure plus pipe capacity is less than the outside pressure. $(P_1 + P_a) - P_F \le 0$

	Long Term	Short Term	Differential Pressures
Pull Back	12.36 psi	86.42 psi	Internal Air and External Fluid 1 = $(P_A + P_a) - P_{DF1}$
Pull Back	11.83 psi	85.89 psi	Internal Air and External Fluid 2 = $(P_A+P_a)-P_{DF2}$
Pull Back	28.80 psi	102.86 psi	Internal Ballasted and External Fluid 1 = $(P_B+P_a)-P_{DF1}$
Pull Back	28.28 psi	102.34 psi	Internal Ballasted and External Fluid 2 = $(P_B+P_a)-P_{DF2}$
Long Term	32.92 psi	106.97 psi	Internal Ballasted and External Water = $(P_B+P_a)-P_W$
Operation	16.47 psi	90.53 psi	Internal Air and External Water = $(P_A+P_a)-P_W$

Pull Back Condition - Option 1
Pull Back Condition - Option 2
Pull Back Condition - Option 3
Pull Back Condition - Option 4
Long Term Operating Conditions

Operational Dewatering NO SOIL LOADS

ASSESSMENT UNCONSTRAINED BUCKLING ALONG DRILL PATH BY DIFFERENTIAL PRESSURE

Pipe installation pressure differential does not require ballasting the pipe during pull-back

Pipe may be fully dewatered for operational conditions providing there is no soil loading. Soil loads not assessed.

Engineer to assess any dewatering of the pipe in the future for stability based on actual project conditions and time duration.

D-\CHPE\THDD#73A-74 CIR #2 APC 040124 xishiC

Pg 3 of 3 **HDPE PROPERTIES**

Champlain Hudson Power Express

Segment 8 (Pkg. 5A) - CSX: Roterdam to Bethlehem

Schenectady County, NY

HDD 73A-74 Conduit #2

NY State Thruway (I-90)

3. ASSESS ULTIMATE PULL STRENGTH (UPS) AND SAFE PULL STRENGTH (SPS)

Source PPI PE Handbook Ch 12 Formula 17 SPS = $\pi^*DF^*(Ty)^*D_0^{2*}((1/DR)-(1/DR^2))$

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Designed Pull Duration Time =	12 hr	Quantity of pipes, C		f pipes, Q =	1
Yield Strength Factor, f _Y =	0.4	Recommended (FS = 2.5) Pull Temperature, F = 73		73 deg.	
Pull Time factor, $f_T =$	1	Plexco Engineering Manual Table 3.	7	•	
Design Factor, DF = $f_T^*f_Y$	0.4	SAFE PULL STRENTH, SPS =	50,200 lb		
Temperature factor, f _{temp} =	1	Ultimate Pull Strength, UPS =	125,499 lb		
Temp Corr Tensile Yield, Ty*f _{temp} =				· 	
Safe Allowable Stress, SAS =	1,400 psi	$SAS = Ty^* f_{temp}^* DF Sugar$	ggested SSAS =	1,150 psi	
Safe Pull Strength, SPS Pipe =	50,200 lb	Useing SSAS = 41,235 lb			

Short Term Critical Unconstrained Buckling Pcr reduced for pull tension, PcrR = Pcr*fr

(ASTM F-1962 EQ. 22)

Pull Duration Time =	12 Hr]	Pcr =	267.4 psi	
SAS =	1,400 psi	Design D	Pepth in DF, $H_{MDF} =$	0.0 ft	
Estimated Maximum Pull Stress, σ_i =	1,150 psi	Design Assumpti	ion as Maximum		•
fr = ((5.57-(r+1.09)^2)^.5)-1.09 =	0.88012				
$r = \sigma_i/2*(SSAS) =$	0.20947		Example fro	m Table T5, σ_i =	482 psi
P _{CRR} =	235.4 psi				
FS =	2.0				
$P_{ACRR} = P_{CRR}/FS =$	117.7 psi	Allowable Reduc	ed Short Term Buc	kling pressure du	ring pull
Internal Ballasted and External Fluid 1 = (F	P _B +P _{ACRR})-P _{DF1}	97.13 psi	Pull Back Condition	n - Option 3	OK as >0
Internal Ballasted and External Fluid 2 = (F	P_B+P_{ACRR})- P_{DF2}	96.61 psi	Pull Back Condition	n - Option 4	OK as >0

ASSESSMENT OF SAFE PULL STRENGTH ON TENSION REDUCED BUCKLING CAPACITY

ACCEPTIBLE Acceptible if differential pressures > 0 for reduced buckling capacity

REFERENCE 1 - Plastic Pipe Institute - Handbook of PE Pipe 2nd Edition

REFERENCE 2 - Plastic Pipe Institute - Handbook of PE Pipe 2nd Edition

Design Factor (fe) to apply to HDB

CHAPTER 6 - TABLE 1-2

REFERENCE 3 - Plexco Engineering Manual Book 3 Ch 3 Table 3.7

Time factor for pull duration, f_T

	f _T	Time factor for pull	
	1.00	Up to 1 hour pull	1
	0.95	Up tp 12 hours pull	12
over	0.91	Up to 24 hours	24

